

Equipment Sizing Based on Heuristics

Size does matter

James Cameron

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$$V = 2 \left[\frac{F_L \tau}{\rho_L} \right]$$

F_L liquid flow rate leaving the vessel

ρ_L density of liquid

τ residence time (5 minutes)

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- The aspect ratio $\frac{L}{D} = 4$.

This ratio is **optimal** if bottom and top heads are 4 times as expensive as sides.

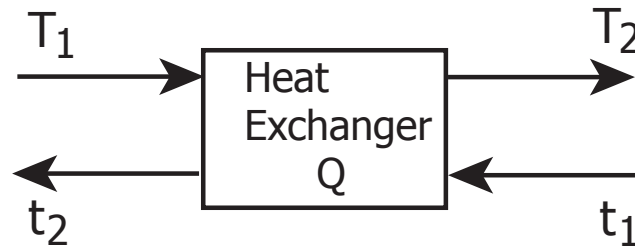
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- For desired temperature range, consider the required material of construction.

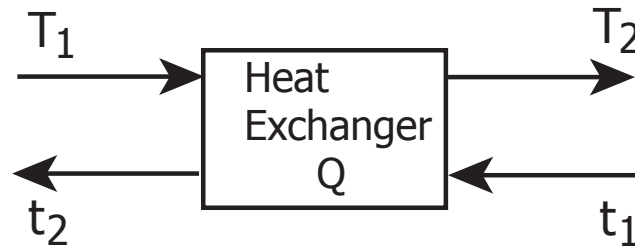
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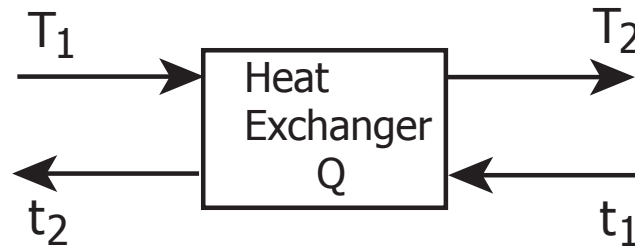
- Heat transfer area can be found from:

$$Q = U A \Delta T_{lm}$$

where

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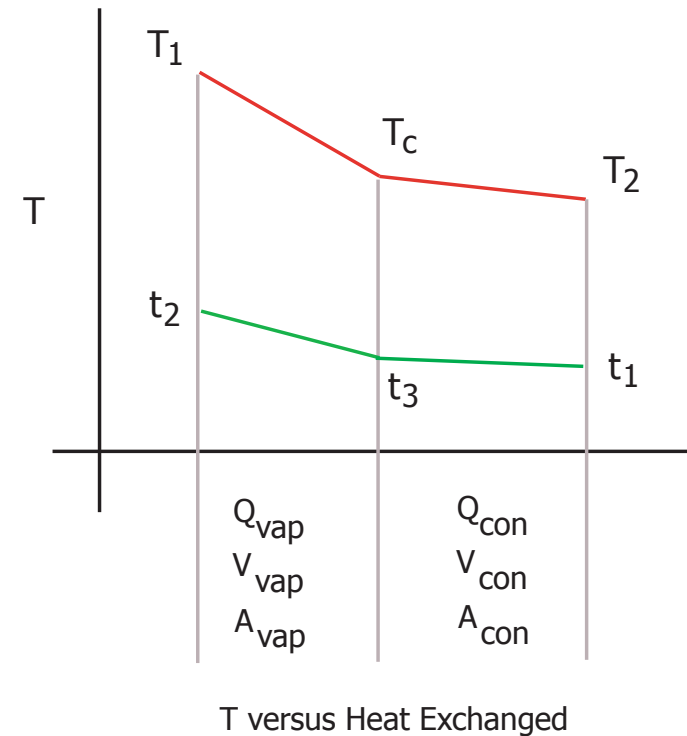
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- The overall heat transfer coefficient, U , can be estimated from heuristics or from standard references (e.g. Perry's Handbook)

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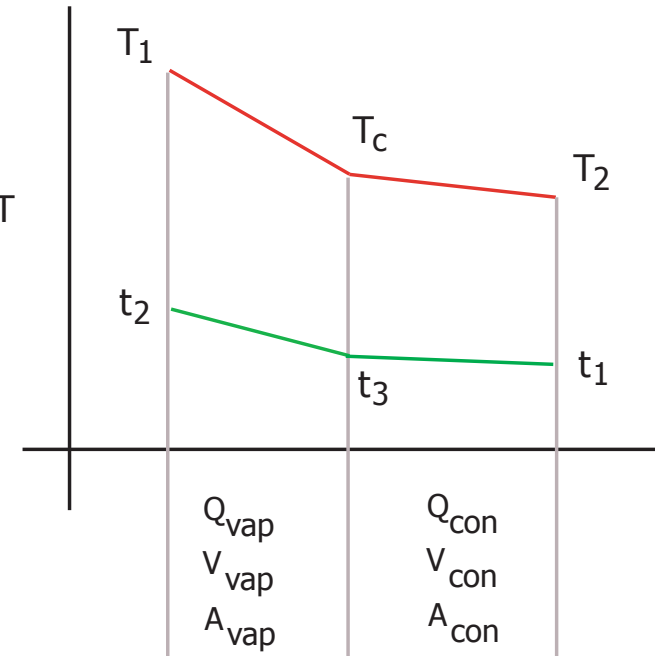
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$$A_{vap} = \frac{Q_{vap}}{U_{vap} \Delta T_{lm}^a}$$

$$\text{where } \Delta T_{lm}^a = \frac{(T_1 - t_2) - (T_c - t_3)}{\ln \left[\frac{T_1 - t_2}{T_c - t_3} \right]}$$

$$A_{con} = \frac{Q_{con}}{U_{con} \Delta T_{lm}^b}$$

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T versus Heat Exchanged

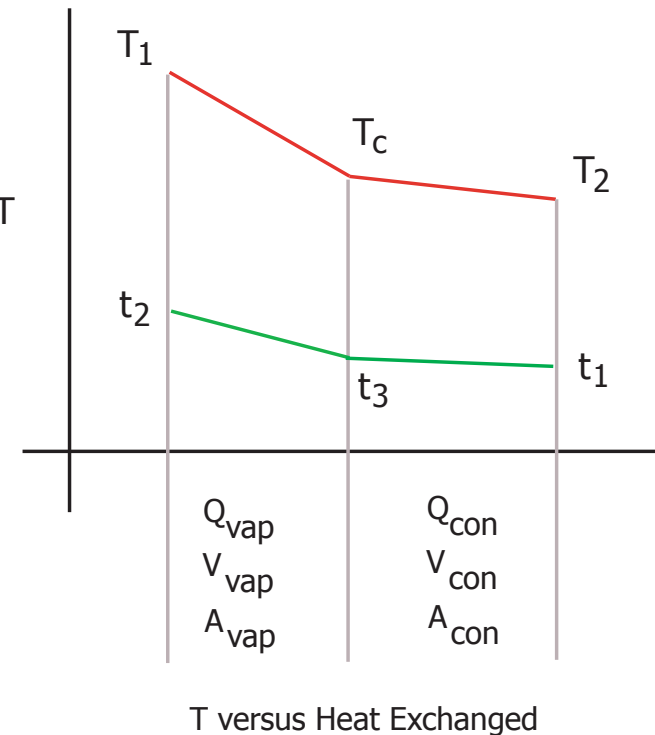
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- We choose 10,000 *sq. ft.* as the **maximum** exchanger area. If more area is required, **multiple** heat exchangers in **parallel** are used.

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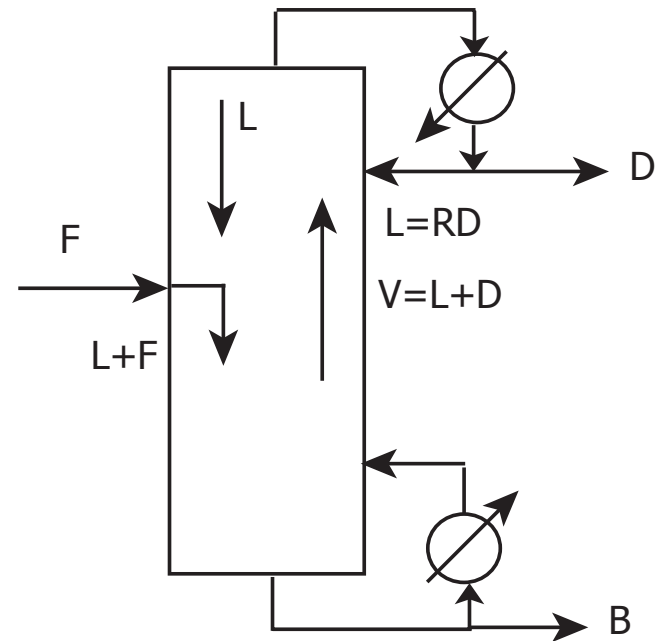
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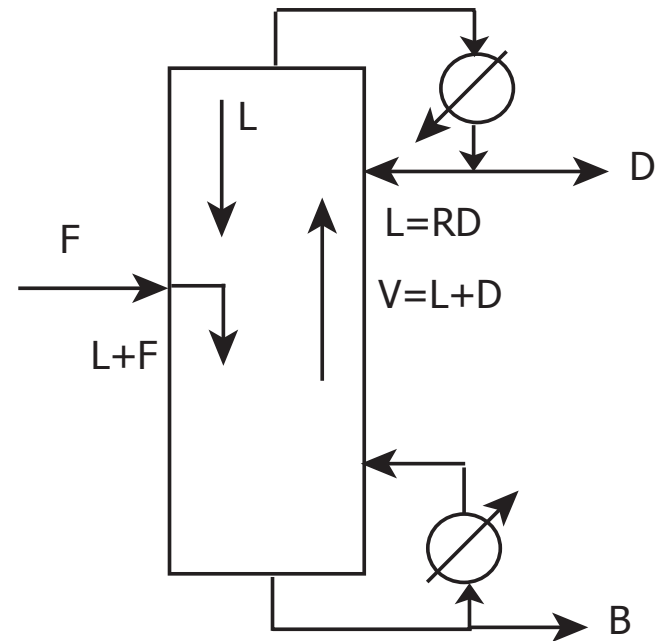
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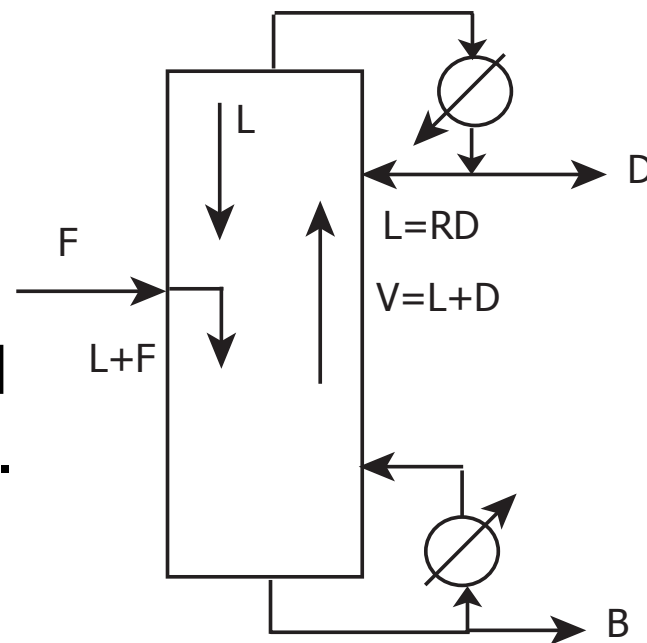


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At the flooding velocity, the vapor flow rate is so high that no net liquid flow occurs and **entrainment** begins.

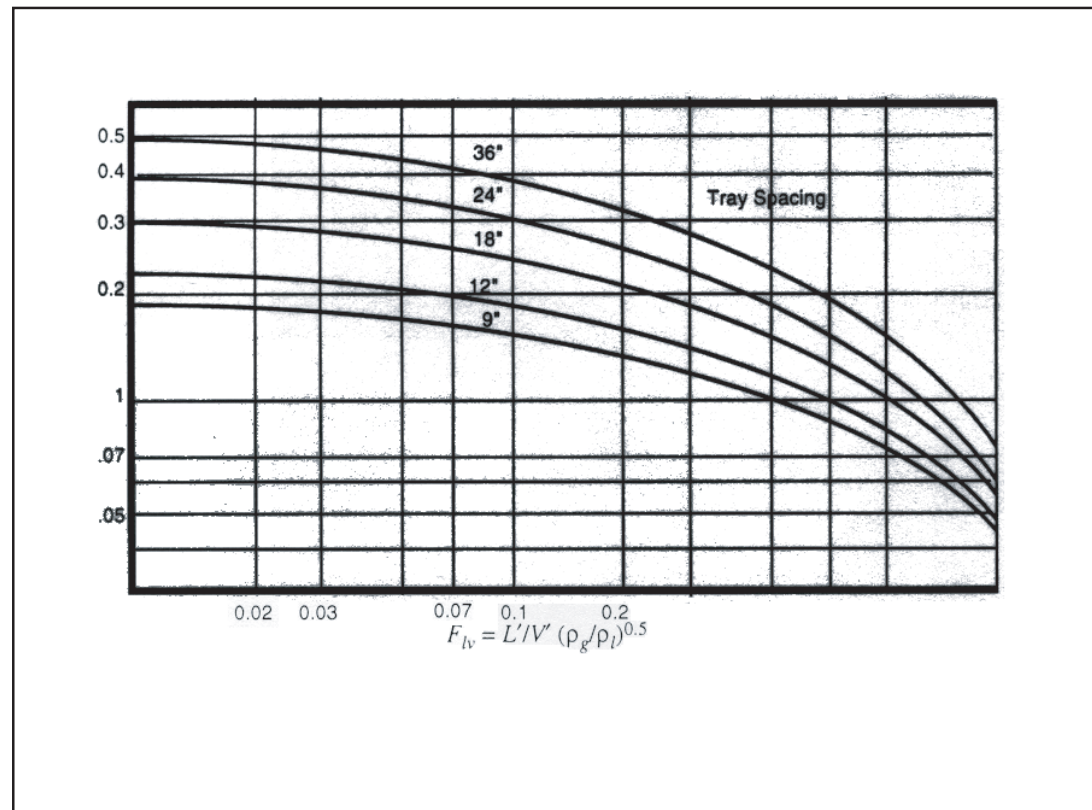


- Calculate dimensionless flow parameter F_{lv}

$$F_{lv} = \frac{L'}{V'} \left(\frac{\rho_g}{\rho_l} \right)^{0.5}$$

where $\frac{L'}{V'}$ is the liquid/gas mass ratio at the point of consideration and $\frac{\rho_g}{\rho_l}$ is the gas/liquid density ratio.

- Calculate capacity parameter $C_{sb,f}$ from the chart below for a given tray spacing:



- Calculate linear flooding velocity (ft/s) from

$$U_{nf} = C_{sb,f} \left(\frac{\rho_l - \rho_g}{\rho_g} \right)^{0.5} \left(\frac{\sigma}{20} \right)^{0.2}$$

where ρ_g and ρ_l are the gas and liquid mass densities and σ is the liquid surface tension in *dynes/cm*.

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- Calculate area of cross-section from $A = \frac{V'}{0.8U_{nf}\epsilon\rho_g}$

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If $D > 20 \text{ ft}$, then **split** the column into two columns running in **parallel**.

- The number of actual trays is given by $\frac{N_T}{\eta}$ where the efficiency is assumed to be 80%. Assume a tray spacing of 24" to calculate **column height**.

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- Calculate heat duties for condenser and reboiler from energy balance.