# Qualitative Effect of P, PI, PID parameters

So far in this course, we have done the following:

- Developed dynamic models for chemical processes
- Studied the effect of changing inputs on the outputs and states
- Developed a procedure for interconnection of systems

In this lecture, we will address the issue of what happens when we connect a controller to a process. In particular, we will study how the parameters of the controller (which we can tune), affect the outputs.

# P Controller

## Consider the following process:

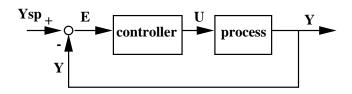
$$\frac{d}{dt} \begin{bmatrix} X_1 \\ X_2 \\ X_3 \end{bmatrix} = \begin{bmatrix} -1 & 0 & 0 \\ 1 & -1 & 0 \\ 0 & 10 & -10 \end{bmatrix} \begin{bmatrix} X_1 \\ X_2 \\ X_3 \end{bmatrix} + \begin{bmatrix} 1 \\ 0 \\ 0 \end{bmatrix} U$$

$$Y = \begin{bmatrix} 0 & 0 & 1 \end{bmatrix} \begin{bmatrix} X_1 \\ X_2 \\ X_3 \end{bmatrix}$$
(1)

## and the P controller

$$U = k_c E$$

$$= k_c (Y_{sp} - Y)$$
(2)

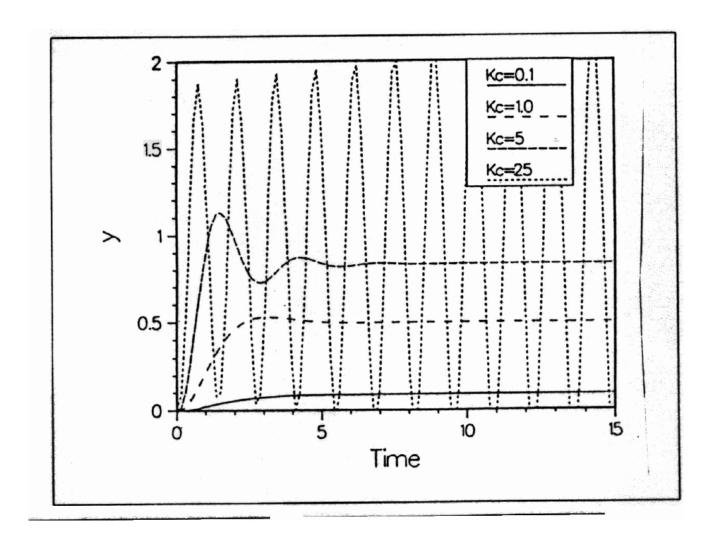


The closed-loop system is given by

$$\frac{d}{dt} \begin{bmatrix} X_1 \\ X_2 \\ X_3 \end{bmatrix} = \begin{bmatrix} -1 & 0 & -k_c \\ 1 & -1 & 0 \\ 0 & 10 & -10 \end{bmatrix} \begin{bmatrix} X_1 \\ X_2 \\ X_3 \end{bmatrix} + \begin{bmatrix} k_c \\ 0 \\ 0 \end{bmatrix} Y_{sp}$$

$$Y = \begin{bmatrix} 0 & 0 & 1 \end{bmatrix} \begin{bmatrix} X_1 \\ X_2 \\ X_3 \end{bmatrix} \tag{3}$$

Suppose  $Y_{sp}$  undergoes a step change from 0 to 1. Clearly, we would like Y to reach the new value of the setpoint as soon as possible. What is the effect of the value of  $k_c$  on the output Y?



- For small  $k_c$ , response is smooth and stable, but there is a large off-set.
- For medium  $k_c$ , response is oscillatory and stable, but the off-set is small.
- For large  $k_c$ , the response is oscillatory and unstable.

# PI Controller

## Consider the following process:

$$\frac{d}{dt} \begin{bmatrix} X_1 \\ X_2 \\ X_3 \end{bmatrix} = \begin{bmatrix} -1 & 0 & 0 \\ 1 & -1 & 0 \\ 0 & 10 & -10 \end{bmatrix} \begin{bmatrix} X_1 \\ X_2 \\ X_3 \end{bmatrix} + \begin{bmatrix} 1 \\ 0 \\ 0 \end{bmatrix} U$$

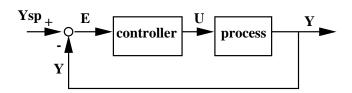
$$Y = \begin{bmatrix} 0 & 0 & 1 \end{bmatrix} \begin{bmatrix} X_1 \\ X_2 \\ X_3 \end{bmatrix}$$
(4)

(4)

#### and the PI controller

$$\frac{dX_4}{dt} = Y_{sp} - Y$$

$$U = k_c E + \frac{k_c}{\tau_I} X_4$$
(5)



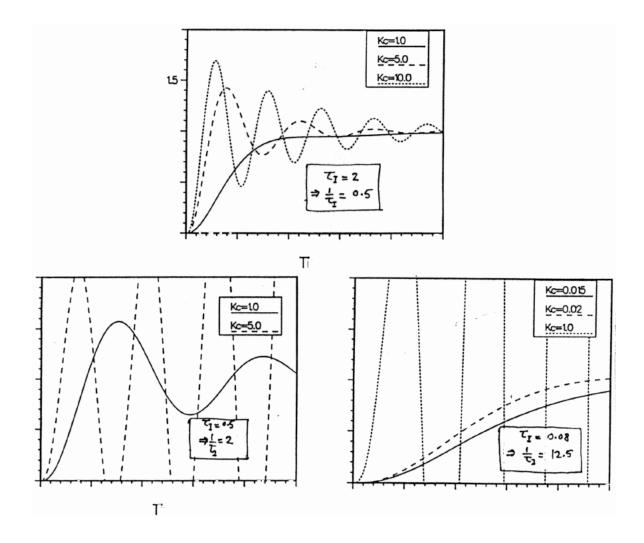
The closed-loop system is given by

$$\frac{d}{dt} \begin{bmatrix} X_1 \\ X_2 \\ X_3 \\ X_4 \end{bmatrix} = \begin{bmatrix} -1 & 0 & -k_c & \frac{k_c}{\tau_I} \\ 1 & -1 & 0 & 0 \\ 0 & 10 & -10 & 0 \\ 0 & 0 & -1 & 0 \end{bmatrix} \begin{bmatrix} X_1 \\ X_2 \\ X_3 \\ X_4 \end{bmatrix} + \begin{bmatrix} k_c \\ 0 \\ 0 \\ 1 \end{bmatrix} Y_s$$

$$Y = \begin{bmatrix} 0 & 0 & 1 & 0 \end{bmatrix} \begin{bmatrix} X_1 \\ X_2 \\ X_3 \\ X_4 \end{bmatrix}$$

(6)

Suppose  $Y_{sp}$  undergoes a step change from 0 to 1. Clearly, we would like Y to reach the new value of the setpoint as soon as possible. What is the effect of the value of  $k_c$  and  $\tau_I$  on the output Y?



• Integral action eliminates off-set.

• As  $\tau_I$  is decreased (=>  $\frac{1}{\tau_I}$  is increased), the range of values for  $k_c$  which lead to stable output response, decreases.

# PID Controller

## Consider the following process:

$$\frac{d}{dt} \begin{bmatrix} X_1 \\ X_2 \\ X_3 \end{bmatrix} = \begin{bmatrix} -1 & 0 & 0 \\ 1 & -1 & 0 \\ 0 & 10 & -10 \end{bmatrix} \begin{bmatrix} X_1 \\ X_2 \\ X_3 \end{bmatrix} + \begin{bmatrix} 1 \\ 0 \\ 0 \end{bmatrix} U$$

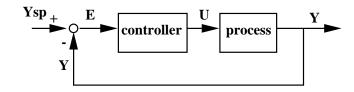
$$Y = \begin{bmatrix} 0 & 0 & 1 \end{bmatrix} \begin{bmatrix} X_1 \\ X_2 \\ X_3 \end{bmatrix}$$
(7)

### and the PID controller

$$\frac{dX_4}{dt} = E$$

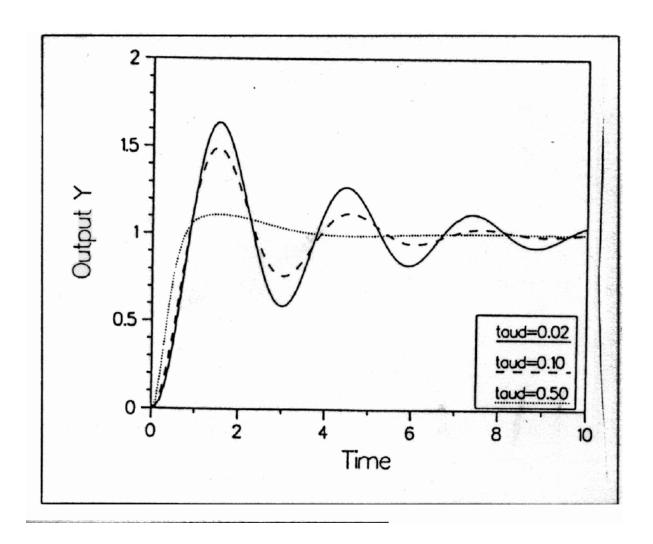
$$\frac{dX_5}{dt} = -\frac{1}{\alpha \tau_D} X_5 + \frac{1}{\alpha \tau_D} E \tag{8}$$

$$U = k_c(1+\frac{1}{\alpha})E + \frac{k_c}{\tau_I}X_4 - \frac{k_c}{\alpha\tau_D}X_5$$



Suppose  $Y_{sp}$  undergoes a step change from 0 to 1. Clearly, we would like Y to reach the new value of the setpoint as soon as possible. What is the effect of the value of  $k_c$ ,  $\tau_I$ , and  $\tau_D$  on the output Y?

The value of  $\alpha$  is set to 0.1 for most commercial controllers. Thus there are only three parameters to vary  $(k_c, \tau_I, \text{ and } \tau_D)$ 



• Integral action eliminates off-set.

• Derivative action has a stabilizing effect on the process. Thus, the presence of the  $\tau_D$  term allows the use of higher values of  $k_c$  as compared to the PI controller.

# Summary

- Proportional action alone is not sufficient to tightly control the output to the desired set-point. Increasing  $k_c$  reduces offset but destabilizes the process.
- Integral action eliminates offset. However as the integral term becomes larger ( $\tau_I$  becomes small), the response is destabilized.
- Derivative action has a stabilizing effect on the closed-loop system which allows for higher values of proportional and integral terms to be used for faster response.