- 1. A piston/cylinder assembly (with an initial volume of $V_1=0.1 \text{ m}^3$, $P_1=1 \text{ MPa}$) contains 1 kg of a mixture of saturated liquid water and saturated steam as shown. The system is undergoing through four processes 1-2-3-4-1 as indicated on the T-v diagram. 2-3 and 4-1 are constant volume process. (40%)
 - (a) Determine the initial quality (x_1) and temperature (T_1) ;
 - (b) determine the temperature (T_2) at the state 2;
 - (c) determine the quality (x_4) and temperature (T_4) at the state 4;
 - (d) determine the amount of the heat transfer Q_{12} added and work done W_{12} during the process 1-2;
 - (e) determine the amount of the heat transfer Q_{23} lost and work done W_{23} during the process 2-3.



(a)
$$v_1 = \frac{0.1}{1} = 0.1 m^3 / kg, P_1 = 1 MPa, T_1 = 179.9^{\circ}C$$

From saturated steam table : $v_{f,1} = 0.001127$, $v_{g,1} = 0.1944$

$$v_1 = v_{f,1} + x_1(v_{g,1} - v_{f,1}), \quad x_1 = \frac{0.1 - 0.001127}{0.1944 - 0.001127} = 0.51$$

(b)
$$P_3 = 0.3MPa$$
, from saturation steam table : $v_{g,3} = 0.6058 = v_2 > v_{g,3}$

Use superheated table and interpolate between 1,000°C & 1,100°C : $P_2 = 1MPa$, $v_2 = 0.6058(m^3 / kg)$

$$T_2 = 1000 + \frac{1100 - 1000}{0.6335 - 0.5871} (0.6058 - 0.5871) = 1040.3(^{\circ}C)$$

(c)
$$T_4 = 133.55$$
 °C from saturation steam table with $P_4 = 0.3MPa$
 $v_{f,4} = 0.001073, v_{g,4} = 0.6058, v_4 = v_1 = 0.1m^3 / kg$ (constant volume process)
 $x_4 = \frac{0.1 - 0.001073}{0.001073} = 0.165$

$$-\frac{1}{0.6058-0.001073}$$

(d)
$$W_{12} = \int_{1}^{2} P dV = P_1(V_2 - V_1) = P_1 m(v_2 - v_1) = (1000)(1)(0.6058 - 0.1) = 505.8(kJ)$$

 $\Delta U_{12} = U_2 - U_1 = m(u_2 - u_1) = Q_{12} - W_{12}$
 $u_1 = u_{f,1} + x_1 u_{fg,1} = 761.68 + (0.51)(1822) = 1690.9$, from saturated steam table
 u_2 needs to be interpolated from the superheated table between 1,000°C and 1,100°C
 $u_2 = 4050.5 + \frac{4255.1 - 4050.5}{1100 - 1000} (1040 - 1000) = 4132.3(kJ / kg)$
 $Q_{12} = (1)(4132.3 - 1690.9) + 505.8 = 2947.2(kJ)$

(e)
$$W_{23} = \int_{2}^{3} P dV = 0$$

 $\Delta U_{23} = m(u_3 - u_2) = Q_{23}$
 $Q_{23} = m(u_{g,3} - u_2) = (1)(2543.6 - 4132.3) = -1588.7(kJ);$
 $u_{g,3}$ from saturated steam table with P = 0.3 MPa

- 2. The cylinder/piston assembly is filled with 1 kg of air (an ideal gas with R=0.287 kJ/kg K and C_v =0.72 kJ/kg, k=1.4.) The initial pressure inside the cylinder is P₁=100 kPa. The system is going through three processes 1-2-3-1 to complete a cycle as shown. (1-2:constant pressure and its volume expands from 1 m³ to 2 m³; 2-3: constant volume; 3-1: adiabatic.) (30%)
 - (a) Determine the temperatures at all states $(T_1, T_2 \& T_3)$;
 - (b) determine the work (W_{12}) and the heat transfer (Q_{12}) between 1 and 2;
 - (c) determine the work (W_{23}) and the heat transfer (Q_{23}) between 2 and 3;
 - (d) determine the work (W_{31}) between 3 and 1.



From1 - 2 : constant prerssure

(b)
$$W_{12} = \int_{1}^{2} PdV = P_1(V_2 - V_1) = (100)(2 - 1) = 100(kJ)$$

(a) $T_1 = \frac{P_1V_1}{mR} = \frac{(100)(1)}{(1)(0.287)} = 348(K)$
(a) $T_2 = \frac{P_2V_2}{mR} = \frac{(100)(2)}{(1)(0.287)} = 697(K)$
(b) $\Delta U_{12} = U_2 - U_1 = mC_V(T_2 - T_1) = (1)(0.72)(697 - 348) = Q_{12} - W_{12} = Q_{12} - 100$
 $Q_{12} = 351.2(kJ)$
(c) $W_{23} = \int_{2}^{3} PdV = 0$ No external work
From 3 to 1, adiabatic process: $\left(\frac{T_3}{m}\right) = \left(\frac{V_1}{V_1}\right)^{k-1}, \frac{T_3}{240} = \left(\frac{1}{2}\right)^{1.4-1} = 0.758$

$$(T_{1}) (V_{3}) , 348 (2)$$

$$(a) T_{3} = 263.7(K)$$

$$(c) \Delta U_{23} = mC_{V}(T_{3} - T_{2}) = Q_{23} - W_{23}$$

$$Q_{23} = (1)(0.72)(263.7 - 697) + 0 = -311.9(kJ)$$

$$(d) \text{ Adiabatic process} Q_{31} = 0$$

$$\Delta U_{31} = Q_{31} - W_{31}$$

$$W_{31} = -\Delta U_{31} = mC_{V}(T_{3} - T_{1}) = (1)(0.72)(263.7 - 348) = -60.7(kJ)$$