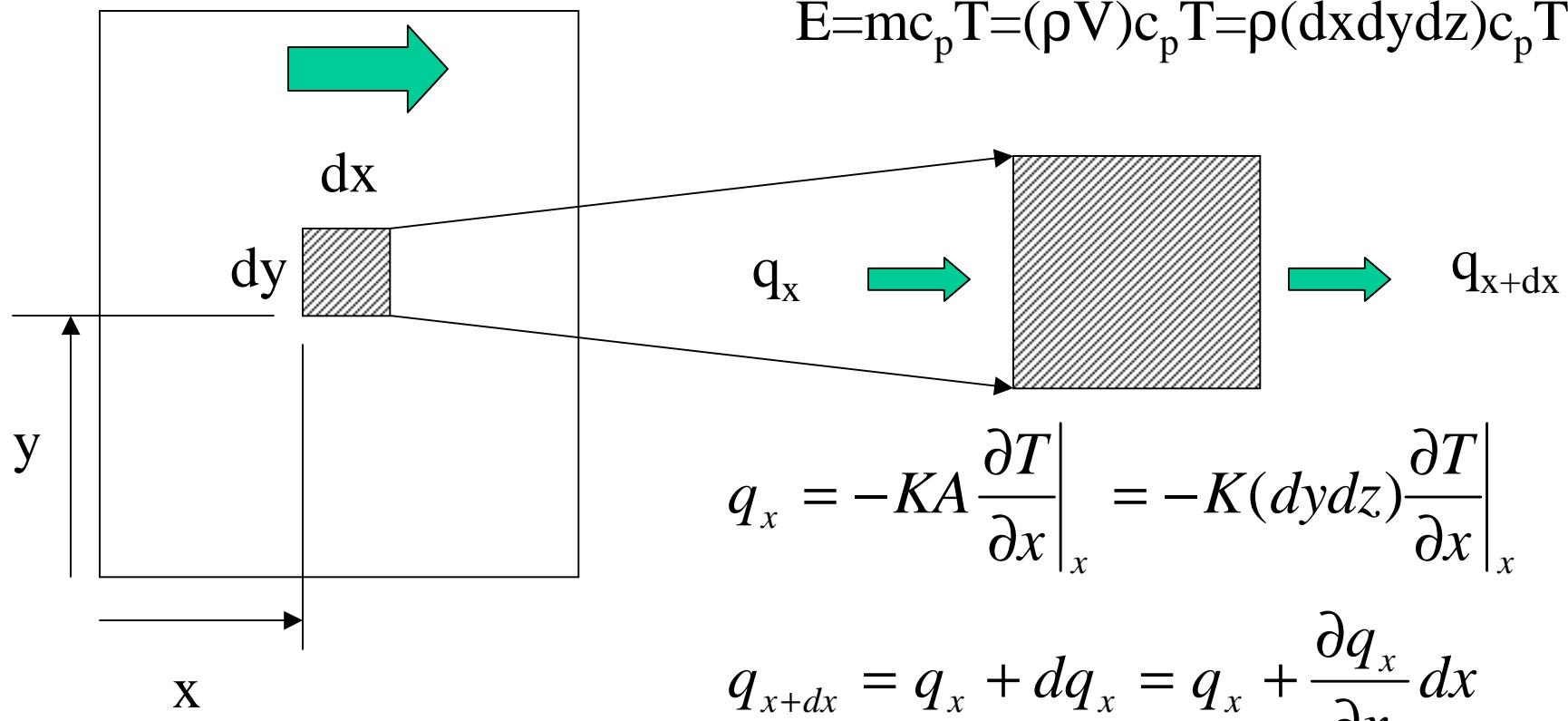


Heat Diffusion Equation

Energy balance equation: $\frac{dE}{dt} = \frac{dE_g}{dt} + q_{in} - q_{out} + \dot{E}_1 - \dot{E}_2 - \frac{dW}{dt}$

All go to zero

Apply this equation to a solid undergoing conduction heat transfer:



Heat Diffusion Equation (2)

Energy Storage = Energy Generation + Net Heat Transfer

$$\frac{\partial}{\partial t}(\rho c_p T) dxdydz = \dot{q} dxdydz + q_x - q_{x+dx}$$

$$\rho c_p \frac{\partial T}{\partial t} dxdydz = \dot{q} dxdydz + q_x - (q_x + \frac{\partial q_x}{\partial x} dx)$$

$$= \dot{q} dxdydz - \frac{\partial}{\partial x} (-k \frac{\partial T}{\partial x}) dxdydz$$

$$\rho c_p \frac{\partial T}{\partial t} = \dot{q} + \frac{\partial}{\partial x} (k \frac{\partial T}{\partial x}) + \boxed{\frac{\partial}{\partial y} (k \frac{\partial T}{\partial y}) + \frac{\partial}{\partial z} (k \frac{\partial T}{\partial z})}$$

Note: partial differential operator
is used since $T=T(x,y,z,t)$

Generalized to three-dimensional

Heat Diffusion Equation (3)

$$\rho c_p \frac{\partial T}{\partial t} = \dot{q} + \frac{\partial}{\partial x} (k \frac{\partial T}{\partial x}) + \frac{\partial}{\partial y} (k \frac{\partial T}{\partial y}) + \frac{\partial}{\partial z} (k \frac{\partial T}{\partial z})$$

Special case 1: no generation $\dot{q} = 0$

Special case 2: constant thermal conductivity $k = \text{constant}$

$$\rho c_p \frac{\partial T}{\partial t} = k \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} \right) + \dot{q} = k \nabla^2 T + \dot{q},$$

where $\nabla^2 = \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial y^2} + \frac{\partial^2}{\partial z^2}$ is the Laplacian operator

Special case 3: $\frac{\partial}{\partial t} = 0$ and $\dot{q} = 0$

$$\nabla^2 T = \frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} = 0, \text{ The famous Laplace's equation}$$

1-D, Steady Heat Transfer

Assume steady and no generation, 1 - D Laplace' s equation

$$\frac{d^2T}{dx^2} = 0, T(x, y, x, t) = T(x), \text{ function of } x \text{ coordinate alone}$$

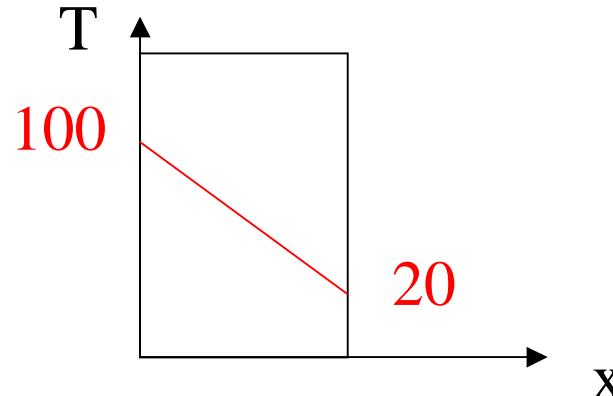
Note: ordinary differential operator is used since $T = T(x)$ only

The general solution of this equation can be determined by integrating twice:

First integration leads to $\frac{dT}{dx} = \text{constant} = C_1$.

Integrate again $T(x) = C_1 x + C_2$

Second order differential equation: need two boundary conditions to determine the two constants C_1 and C_2 .



$$T(x=0)=100^\circ\text{C}=C_2$$

$$T(x=1 \text{ m})=20^\circ\text{C}=C_1+C_2, C_1=-80^\circ\text{C}$$

$$T(x)=100-80x \text{ } (\text{ }^\circ\text{C})$$

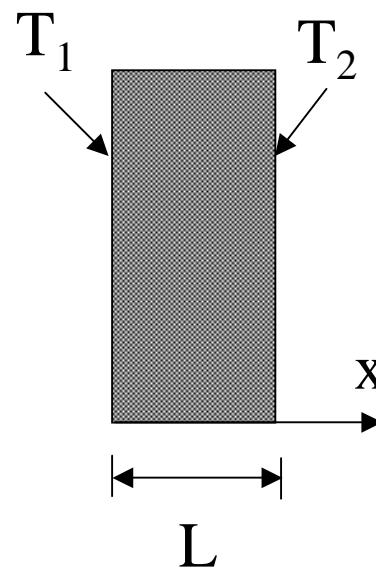
1-D Heat Transfer (cont.)

Recall Fourier's Law:

$$q = -kA \frac{dT}{dx}, \text{ If the temperature gradient is a constant}$$

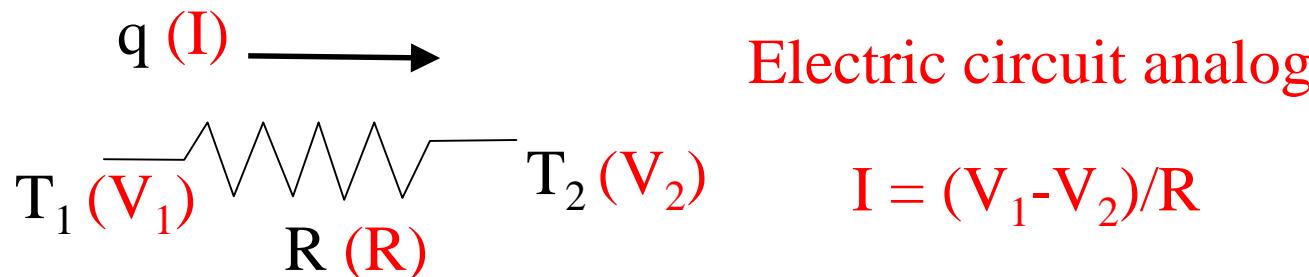
$q = \text{constant}$ (heat transfer rate is a constant)

$$\frac{dT}{dx} = \frac{T_2 - T_1}{L}, \text{ where } T(x=0) = T_1, T(x=L) = T_2$$

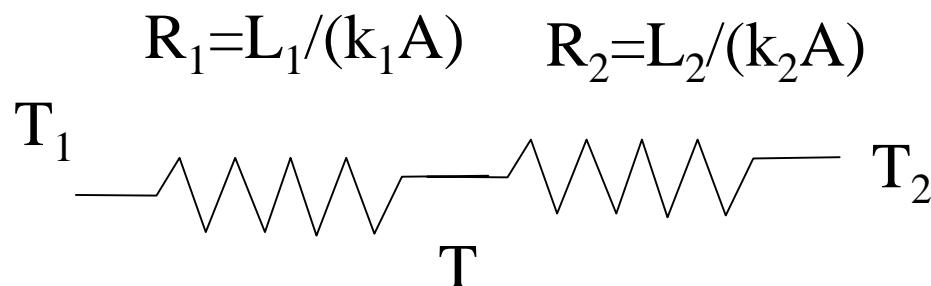
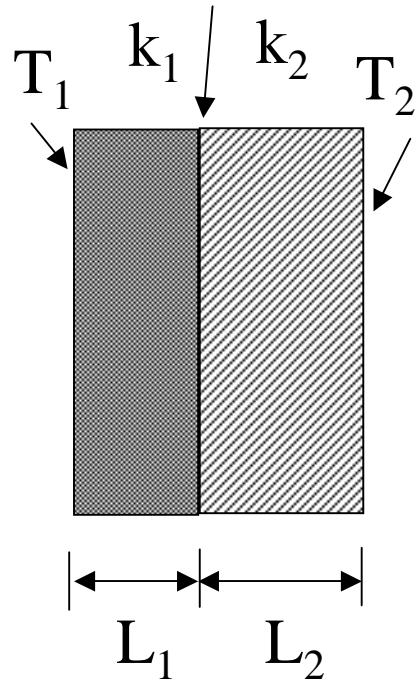


$$q = -kA \frac{dT}{dx} = kA \frac{T_1 - T_2}{L} = \frac{T_1 - T_2}{(L / kA)}$$

$$q = \frac{T_1 - T_2}{R}, \text{ where } R = \frac{L}{kA} : \text{thermal resistance}$$



T Composite Wall Heat Transfer



$$q = \frac{T_1 - T_2}{R} = \frac{T_1 - T_2}{R_1 + R_2} = \frac{T_1 - T_2}{\left(\frac{L_1}{k_1 A}\right) + \left(\frac{L_2}{k_2 A}\right)}$$

$$\text{Also, } q = \frac{T_1 - T}{R_1}, \quad T = T_1 - qR_1 = T_1 - q\left(\frac{L_1}{k_1 A}\right)$$

Note: In the US, insulation materials are often specified in terms of their thermal resistance in $(\text{hr ft}^2 \text{ }^\circ\text{F})/\text{Btu}$ ----> 1 Btu=1055 J.
 R-value = L/k , R-11 for wall, R-19 to R-31 for ceiling.

R value

The thermal resistance of insulation material can be characterized by its R-value. R is defined as the temperature difference across the insulation by the heat flux going through it:

$$R = \frac{\Delta T}{q''} = \frac{\Delta T}{k \frac{\Delta T}{\Delta x}} = \frac{\Delta x}{k}$$

The typical space inside the residential frame wall is 3.5 in. Find the R-value if the wall cavity is filled with fiberglass batt. ($k=0.046 \text{ W/m.K}=0.027 \text{ Btu/h.ft.R}$)

$$R = \frac{\Delta x}{k} = \frac{0.292 \text{ ft}}{0.027 \text{ Btu / h. ft. R}} = 10.8(\text{R. ft}^2 \cdot \text{h / Btu}) \approx R - 11$$