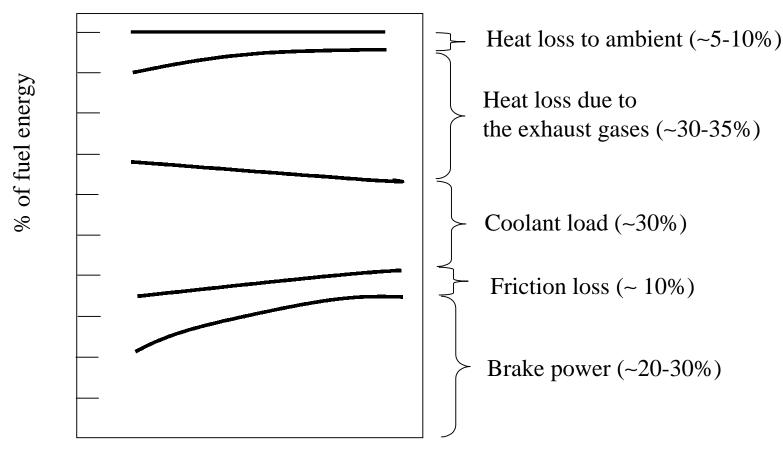
Engine Heat Transfer

➤ Engine heat transfer is an important design consideration for many practical reasons.

- Emission control: catalytic converter performance (>500 K)
- Charge heating: decrease volumetric efficiency
- Material temperature limitations: thermal barrier, thermal fatigue & stress
- Engine performance: heat loss leads to lower operating temperature \rightarrow lower efficiency
- Lubrication limits: lubricant lose its viscosity, ability to maintain a thin film between surfaces, at high temperature
- > All modes of heat transfer are important
 - Conduction: $q = -kA\nabla T$
 - Convection: $q = hA(T_s T_{\infty})$
 - Radiation: $q = \varepsilon \sigma A (T_s^4 T_{surr}^4)$

Overall Energy Balance

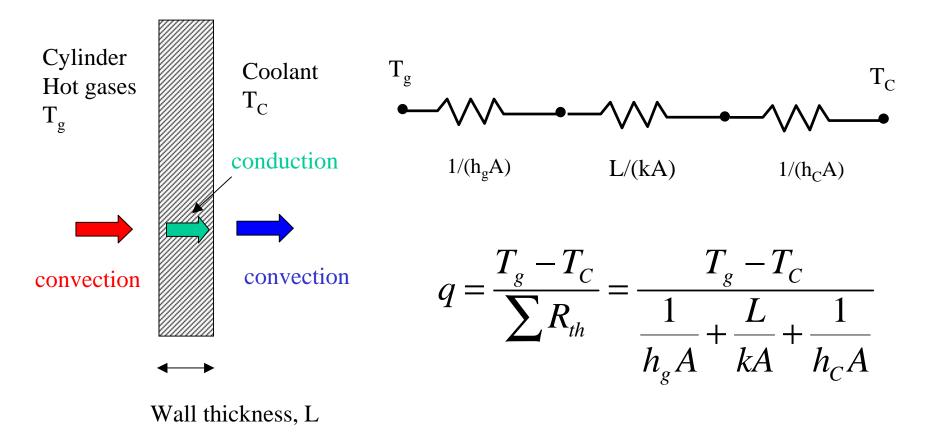


Intake manifold pressure

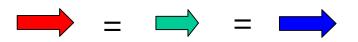
$$\dot{m}_f h_f + \dot{m}_a h_a = P_b + q_{coolant} + q_{ambient} + q_{friction} + (\dot{m}_f + \dot{m}_a) h_e$$

(*T*otal available energy)=(Brake power)+(Other losses)+(exhausted energy)

1-D Heat Transfer Model



Is the steady state assumption valid?



For 1-D, steady state heat transfer

Unsteady Heat Penetration

Now, consider the unsteady nature of the problem since the cylinder wall experiences a periodic heat flux from the inside cylinder wall. The unsteady conduction equation can be written as:

 $\frac{\partial T}{\partial t} = \frac{1}{\rho c_p} \frac{\partial}{\partial x} \left(k \frac{\partial T}{\partial x} \right) = \alpha \frac{\partial^2 T}{\partial x^2}, \text{ by assuming k=constant and } \alpha = \frac{k}{\rho c_p}$ The following boundary and initial conditions have to be satisfied: (1) T=T_L at x=L (Note: this is an assumption to make the problem easier to solve in order to understand the physics of the unsteadiness. In reality, the temperature of the coolant is a constant but the wall is not necessarily a constant. However, the difference is negligible for our case.)

(2)
$$-k\frac{\partial 1}{\partial x} = q_0^{"} + q_1^{"}\sin(\omega t)$$
 at x=0 (Periodic heat flux from the inside of the cylinder.)

(3) $T=T_i(x)$ at t=0 (The initial condition)

Unsteady Heat Penetration

An approximate solution can be derived if the following two conditions

are satisfied: $\omega t \gg 1$ and $\frac{\omega L^2}{2\alpha} \gg 1$. The unsteady temperature field is given as

$$T(x,t) = T_L + \frac{q_0'}{k}(L-x) + \frac{q_1'}{\left(\frac{\alpha}{\omega}\right)^{1/2}} \exp\left[-\left(\frac{\omega}{2\alpha}\right)^{1/2}x\right] \sin\left[\omega t - \left(\frac{\omega}{2\alpha}\right)^{1/2}x - \frac{\pi}{4}\right]$$

$$\Rightarrow \text{The surface temperature } T(x=0,t) = T_L + \frac{q_0^{''}L}{k} + \frac{q_1^{''}}{\left(\frac{\alpha}{\omega}\right)^{1/2}} \sin\left[\omega t - \frac{\pi}{4}\right]$$

It oscillates with the same frequency as the heat flux with a phase shift of $\frac{\pi}{4}$

 \Rightarrow The osciallation vanishes approaching x=L since the oscillatory term

decays as
$$\exp\left[\left(-\frac{\omega}{2\alpha}\right)^{1/2}L\right]$$
 and we know $\frac{\omega L^2}{2\alpha} \gg 1$.

Unsteady Penetration Depth

We can define a penetration depth (δ) as the distance where the amplitude of the oscillation decreases to 10% of the value at the surface.

Therefore, the oscillation term is essentially not important further into the wall.

$$0.1 = \exp\left[-\left(\frac{\omega}{2\alpha}\right)^{1/2}\delta\right], \ \delta = -\ln(0.1)\left(\frac{2\alpha}{\omega}\right)^{1/2} = 2.3\left(\frac{2\alpha}{\omega}\right)^{1/2}$$

In general, this is a small value (in the order of mm).

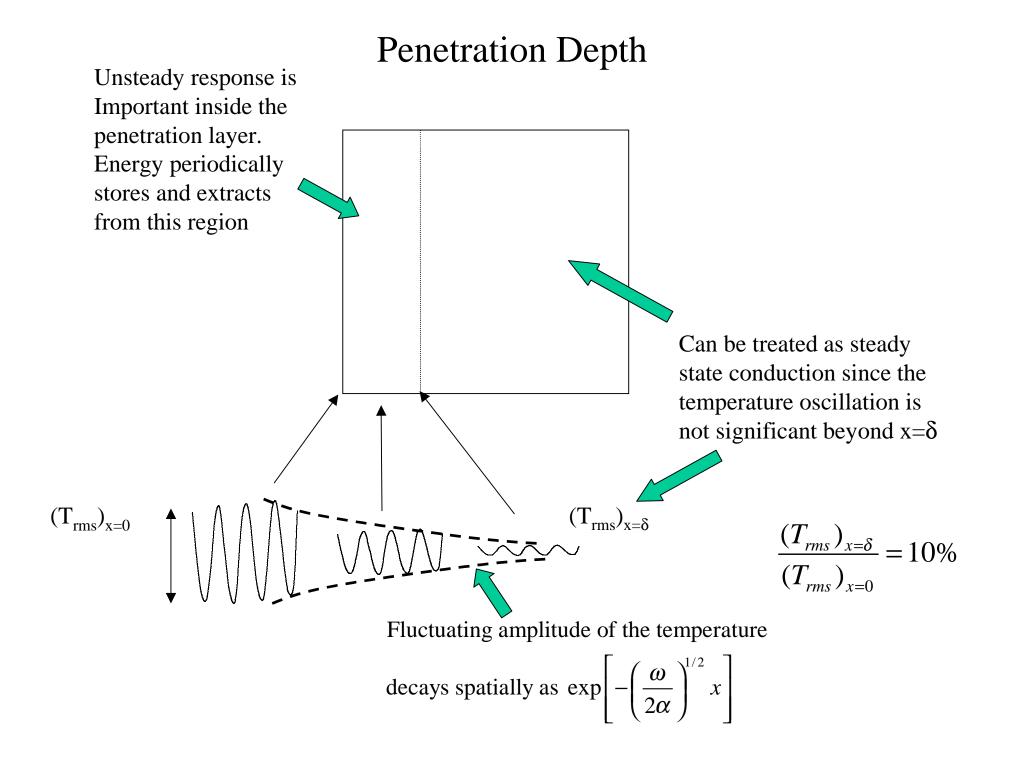
Therefore, only a thin layer close to the inside cylinder wall will actually experience the oscillatory heat flux.

Two simplifications can be introduced:

(1) Beyond x> δ , we can assume steady conduction heat transfer.

(2) The unsteady oscillation can be modelled by using a capacitor to represent

the unsteady response inside the penetration layer (see the following two pages).



Unsteady Heat Model

